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Australian Stock Exchange Limited
Exchange Centre,
Level 6, 20 Bridge Street,
SYDNEY, NSW 2000

SCOPING STUDY BOOSTS BROKEN HILL COBALT PROJECT'S DEVELOPMENT OPTIONS

Highlights

- **Scoping study identifies robust economics for production of sulphuric acid bi-product**
- **Five fast-track, low cost development options identified at nominal processing rates of 1.5 – 7.5 million tonnes per annum**
- **Strong Australian sulphuric acid demand from fertiliser and mineral processing industries**
- **Study enhances project flexibility for development of world-class cobalt mine**
- **First step in ongoing cobalt development, infrastructure and marketing evaluation**

Broken Hill Prospecting Ltd ('BPL' or the 'Company') today announced that a detailed scoping study for the production of sulphuric acid bi-product from its world-class, 100%-owned Broken Hill Cobalt Project in western NSW had highlighted significant potential for a long-term operation with a low capital start-up and staged development.

The study, undertaken by international engineering consultant GHD, confirmed that pyrite from the company's Railway, Pyrite Hill and Big Hill cobalt deposits could yield valuable sulphuric acid bi-product. Currently, sulphuric acid is in strong demand in fertiliser production, mineral processing and other industries. Pyrite treatment would also provide significant cobalt and iron recovery.

BPL's Managing Director, Ian Pringle, said: "This first step towards development of the major Broken Hill Cobalt Project is important because it shows that production of pyrite to produce sulphuric acid could be a valuable revenue stream to support cobalt sales. This outcome gives us considerable flexibility in developing this large project, including how mining should be undertaken and what the end product should be. Next, we need to undertake resource definition, metallurgical studies, mine planning, infrastructure and transport needs and also evaluate the best marketing approach. These project studies will be invaluable in determining how to deliver the best value for BPL shareholders."

Key Points

Staged development could include a combination of the following ore processing options to supply pyrite to a growing market for sulphuric acid with considerable economic benefits from the additional recovery of cobalt and iron;

Start-up production of 1.5 million tonne per year ("Mtpa") of 35% pyrite product from mining, crushing and transportation of high-grade cobalt-pyrite ore.
- Estimated capital cost of A$6.5 million
- Estimated operating cost of A$14.3 million per year
- Benefits include; low capital investment, negligible water use, low power requirement, early cash flow

Flotation processing of 1.5Mtpa of cobalt-pyrite ore feed for production of 300,000tpa of 85-90% pyrite concentrate.
- Estimated capital cost of A$74 million
- Estimated operating cost of A$17.8 million per year

Flotation processing of 7.5Mtpa of cobalt-pyrite ore feed to produce 1.5mtpa of 85-90% pyrite concentrate.
- Estimated capital cost of A$190 million
- Estimated operating cost of A$50.9 million per year
- Potential estimated revenue return for concentrate processing using an established sulphide roast facility is $44 per tonne of ore feed and a 1.6 year pay-back period

Project Strengths

- Located beside railway and road and close to an established mining centre.
- Numerous local markets for pyrite concentrate product as a sulphuric acid source with by-product cobalt and iron ore (Fe-calcine or hematite). These include mineral processing, fertiliser and steel manufacturing industries.
- Potential to export cobalt in concentrate to overseas markets due to good access to port facilities.
- Ability to develop parallel processing streams to supply a variety of pyrite concentrate products into several markets.

Broken Hill Prospecting Limited
ARBN: 003 453 503

Level 14, 52 Phillip Street, Sydney NSW 2000 Box 3486 GPO, Sydney NSW 2001
P: +61 2 9252 5300 F: +61 2 9252 8400 E: info@bhpl.biz W: www.bhpl.biz

Introduction

Broken Hill Prospecting Ltd commissioned GHD* to undertake process scoping studies of possible future development scenarios for the Thackaringa Cobalt Project (Figure 1). The studies investigated recovery of pyrite for off-site generation of sulphuric acid, as well as additional revenue flow for contained cobalt and iron. The results of the work will assist the Company to consider development options for the project based on a nominal ore-process rates ranging between 1.5 - 7.5 Million tonnes per annum (Mtpa).

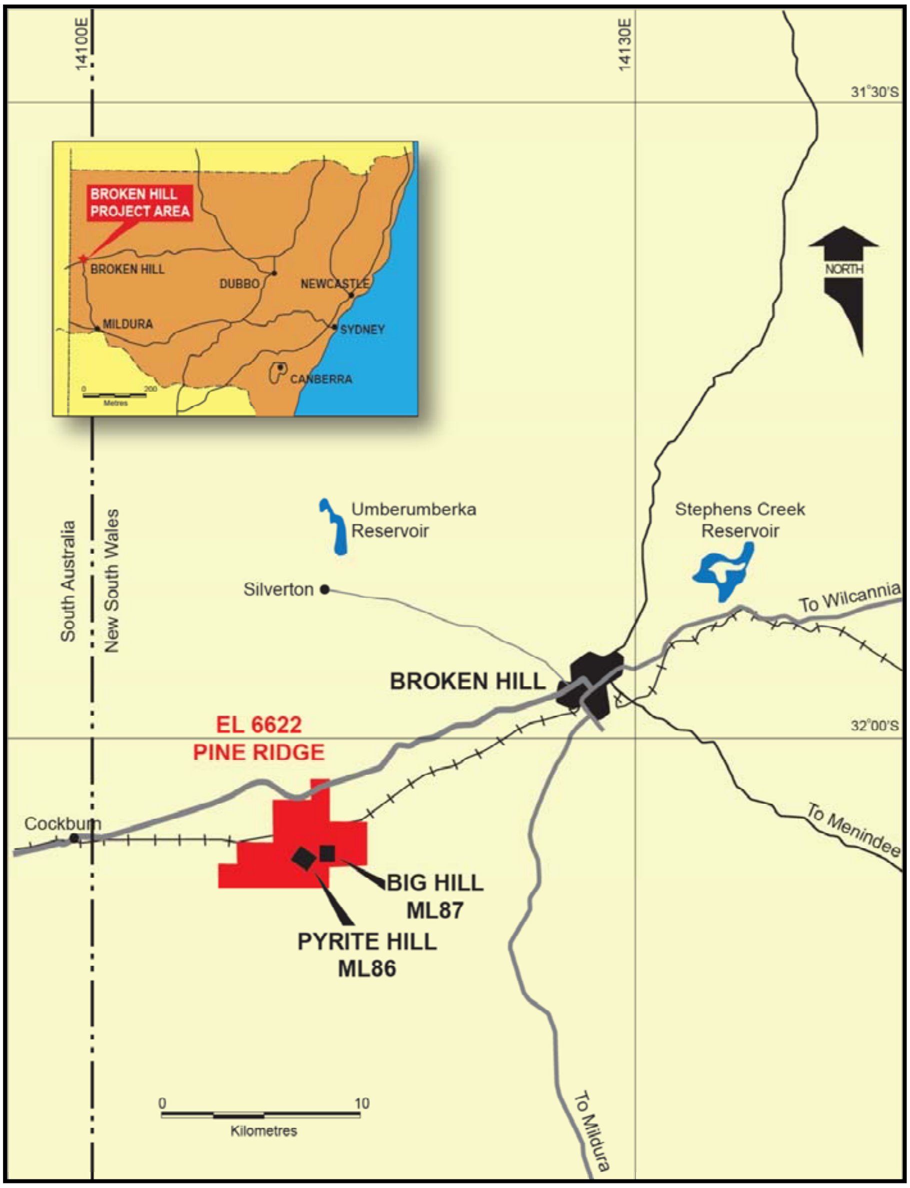

Figure 1. Location of the Thackaringa Cobalt Project

**GHD is an international network of engineers, architects and environmental scientists serving clients in the global markets of water, energy and resources, environment, property and buildings, and transportation. Information on GHD can be found at the GHD website at www.ghd.com/ghd-australia/.*

Options investigated by GHD include:

1. Crush/grind/flotation/dewatering for both 1.5Mtpa and 7.5Mtpa throughput
2. High-grade ore. Crushing without concentration (1.5Mtpa)
3. Medium grade ore with coarse gravity upgrade (1.5Mtpa)
4. Medium grade ore with coarse and sands gravity upgrading (1.5Mtpa)

The studies provide initial indications of capital and operating costs (CAPEX and OPEX) of possible future development scenarios for the project. They include staged mine development options with early, small scale (1.5Mtpa) direct treatment of high-grade ore which focus on low capital expenditure to establish an early revenue stream by using existing infrastructure. Table 1 lists the basic parameters of each of the process Options which were considered.

All of the known cobaltiferous pyrite mineralisation is located near-surface within an exploration licence (EL6622) and two Mining Leases (ML66 and ML67) and can be mined by open cut methods. Pyrite (FeS_2) can make up most of the rock but it is usually between 10-40%. Other minerals in the host rock (gneiss) consist of quartz and albite (sodium plagioclase feldspar). Pyrite is the only significant sulphide in the rock and it contains almost all of the cobalt.

A recent resource evaluation (refer ASX announcement of 27 July, 2012) estimated the combined Inferred Mineral Resources of the deposits (Pyrite Hill, Big Hill and Railway) as 35.7 million tonnes ("Mt') of pyrite mineralisation with an average grade of 1.85 pound per tonne ("lb/t") of cobalt. In addition, 'Potential' for between 37-59Mt of pyrite mineralisation of similar cobalt grade was estimated. This Potential is conceptual in nature and more drilling is required to further define it and there is no certainty that more drilling will result in up-grade of Potential to Mineral Resource.

As a first step to separate cobalt from the rock in any future development the ore is likely to require concentration of the pyrite by gravity and/or flotation processing methods. The pyrite concentrate can then be further processed on site or sent elsewhere to recover sulphur compounds (to produce sulphuric acid*) and cobalt as well as a high iron residue (Fe-calcine or hematite).

Table 1. Mineral Processing Options Summary

Parameter	Unit	7.5 Option 1a	1.5 Option 1b	1.5 Option 2	1.5 Option 3	1.5 Option 4
Annual ore feed	Mtpa	7.5	1.5	1.5	1.5	1.5
Feed	% pyrite	20.4	20.4	35	18	18
Annual product	Mtpa	1.5	0.3	1.5	0.27	0.26
Product grade	% pyrite	85.8	85.8	35	50	60
Pyrite	% recovery	84.1	84.1	100	50	57.3
Pyrite in concentrate	Mtpa	1.29	0.26	0.53	0.14	0.15

** Background information on sulphuric acid is located on the last page of this report.*

Description of Potential Mineral Processing Scenarios

1. **Option 1 (7.5 Mtpa and 1.5 Mtpa) Crush/Grind/Flotation/Dewater**

This option produces a much higher grade concentrate than other options and was considered for two operations of different size (7.5Mtpa and 1.5Mtpa). Option 1 is the most complex of the processing options which were considered in the studies.

Option 1a 7.5Mtpa throughput

A process plant designed to handle 7.5Mtpa of ore and to produce 1.5Mtpa of pyrite/cobalt concentrate will produce two grades (high and low grade) of concentrate. After crushing and grinding the SAG milled ore is processed through a flotation circuit and dewatered to produce a pyrite/cobalt concentrate with a cobalt grade of about 0.445% Co and either 85% pyrite or 90% pyrite depending on whether the cleaning circuit is activated.

Option 1b 1.5Mtpa throughput

This uses the same process but with 20% of the throughput of Option 1a. It could produce 300,000tpa of fine-grained filtered cake product with a moisture content of 10% and a grade of either 85% pyrite or 90% pyrite if a cleaning circuit is added.

2. **Option 2 - High Grade Crushing Only**

This option provides for a simple crushing circuit with minimal processing. A 35% pyrite rock is mined and ore is crushed to minus 25mm (suitable for transport). This high-grade selected mining operation of whole-of ore could produce 1.5Mtpa of 35% pyrite product to a stockpile ready for loading onto rail transport.

This is the simplest of the processing options investigated by GHD and is reliant on selective mining to achieve the necessary head grade. There is no upgrade in pyrite concentration and there is negligible requirement for process water. Additional benefits could include short establishment time and use of crushing equipment on a hire or contract basis for minimal infrastructure and relatively low investment.

3. **Option 3 - Medium Grade with Coarse Gravity**

Using the same front-end crushing operation as Option 2, medium grade ore (18% pyrite) is fed through a screening process to In-Line Pressure Jigs (“IPJ”). After dewatering the product is drained and loaded on rail cars for transport.

This medium grade coarse gravity option is expected to produce 270,000 tpa of minus 25mm as well as a 2mm 50% pyrite product after drainage on the stockpile. This option provides a low-cost addition to Option 2 in order to allow processing of lower grade ore. Like Option 2, this process does not require significant water.

4. **Option 4 - Medium Grade with Coarse and Sands Gravity**

This also has the same front-end crushing operation as Option 2 and the coarse gravity circuit is essentially the same as for Option 3 except that, instead of a dry fine screen, a wet fine screen of 1 mm is used to remove the fines ahead of the coarse gravity circuit. The screened, undersize fine material is then processed through an IPJ.

This medium-grade coarse and sands gravity operation is expected to produce 260,000 tpa of minus 25mm product as well as 0.3 mm 60% pyrite product ready for loading onto rail transport. Option 4 requires a tailings dam and provides a slightly higher recovery and grade but does not allow for future processing of fine fractions.

Mineral Processing Summary of Results

Only preliminary metallurgical and engineering work has been undertaken prior to the GHD scoping studies and each process option requires considerably more test work. Close-spaced drilling and detailed mine studies are also required to determine mining schedules and open cut pit design during pre-feasibility and feasibility investigations and for these reasons the GHD estimates within the scoping studies have +/-50% accuracy. The results and recommendations of the work are an important step in BPL's growth towards becoming a significant cobalt and industrial mineral producer.

Preliminary investigations were undertaken on local availability of power and water for each option. The project will require about 22MW of power supply at full scale production of Option 1 (7.5Mtpa) and this may be available from the 220kV transmission line between Broken Hill and Mildura or from planned wind farms and solar generation projects in the district. The maximum power requirement for the 1.5Mtpa Options is about 4.4MW at full scale production. Option 2 requires significantly less power than other options.

Availability of on-site groundwater was not investigated and only piped water was considered. The Option 1 (7.5Mtpa) process would require several gigalitres of water a year and the region has the capacity to service this level of demand.

Capital Cost Estimates

GHD estimated indicative total capital requirements by using multipliers of capital equipment costs to calculate total CAPEX for each option. These do not include costs associated with site infrastructure (roads, dams), rail siding/loop, offsite infrastructure, mining equipment, approvals, or project finance/legal costs. Capital cost estimates for each Option are summarised in Table 2.

Table 2. Capital and Operating Cost Estimates

CAPEX/OPEX	Unit	7.5 Option	1.5 Option 1	1.5 Option 2	1.5 Option 3	1.5 Option 4
Capital Cost Estimate*	A$ million	190	74	6.5	11	12
	A$ million per year	50.9	17.8	14.3	17.2	19.9
Operating Cost Estimate*	A$ per tonne ore	6.8	12	9.5	11.5	13
	A$ per tonne concentrate	34	59.5	9.5	63.5	77

** Accuracy +/-50%*

Operating Cost Estimates

Operating costs were estimated for the 7.5Mta Option 1 and each of the 1.5Mtpa Options. Workforce is based at Broken Hill (25km by sealed road) which has good facilities for mine and personnel accommodation and support. OPEX estimates for each option are summarised in Table 2. Details of the estimates are based on the following;

- Process factors; based on process design criteria
- Power costs; estimated from other project studies in the Broken Hill region
- Power consumption; calculated from process design criteria
- Workforce/labour rates; industry standards with allowance for on-costs
- Shift work; industry standards with allowance for three shifts per day
- Maintenance; GHD experience on other projects
- Reagent costs; discussions with suppliers
- Consumables; industry standards
- Water; discussions with Essential Water
- General and Administration; industry standards

Project Value Streams for 7.5Mtpa processing

GHD considered each of the value-adding products (cobalt, sulphuric acid and calcine (Fe_2O_3)) and processing scenarios for product from a 7.5Mtpa plant producing pyrite concentrate. Preliminary assessments were undertaken to determine the importance of these products within separate concentrate processing strategies. Because of the wide variety of assumptions this work is indicative and does not represent financial assessment of viability, however, it does give a comparison of value-adding for each product.

Potential revenue return for a strategy to transport containerised pyrite concentrate to an established mineral processing/sulphide roasting operation is $44/t of ore (Table 3). In this scenario, roasted calcine would be leached and cobalt recovered. The Fe-calcine residue would be transported to port and exported to China. Sulphur dioxide gas (SO_2) would be collected during the pyrite roasting and oxidised to sulphuric acid.

Indicative summary operating costs for this strategy were calculated by GHD as $27/t of ore although this is only an indicative and preliminary assessment until more detailed information on ore processing and better cost estimations are undertaken during future pre-feasibility and feasibility studies.

Table 3. Potential Revenue streams for pyrite concentrate processing.

Product	price used ($/t)	Potential Revenue ($/t ore)
cobalt	$28,630	$11
sulphuric acid	$200	$27
calcine (Fe_2O_3)	$100	$6
total		$44

Mineral Processing Comparisons for 1.5Mtpa Options

Comparison of capital and operating cost estimates for each of the four 1.5Mtpa Options (Table 2) are shown in Figure 2. Clearly, Option 2 has lowest cost estimates for both CAPEX ($6.5 million) and OPEX ($14.3 million per year). It also benefits from negligible water requirement and low power consumption which reduce the need for pipeline and transmission line infrastructure. Option 2 also has an advantage of potential temporary site power generation, negligible environmental impact as well as relatively short set-up and start-up time frames.

Comparison of water and power usage for each of the Options is listed in Table 4.

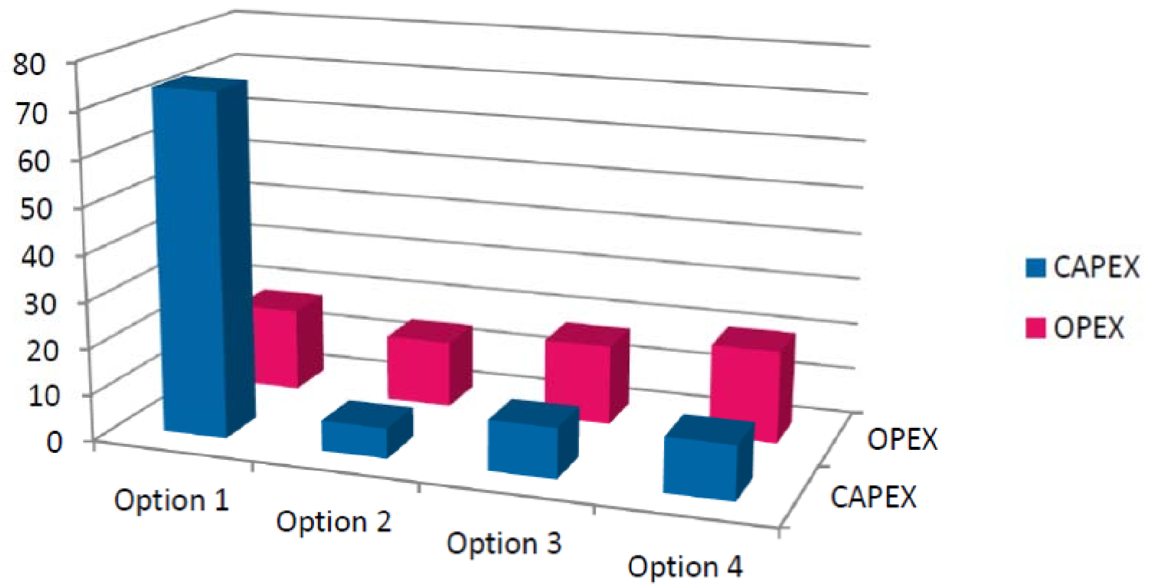

Figure 2. 1.5Mtpa mineral processing options. Comparison of estimated capital and estimated operation costs (scale in A$million).

Table 4. Comparison of power and water requirements

	7.5 Option	1.5 Option 1	1.5 Option 2	1.5 Option 3	1.5 Option 4
Water usage	high	high	low	low	medium
Power usage	high	high	low	low	medium

Roasting of Pyrite Concentrate

A summary of sulphide roasting, requirements and conditions were described by GHD in order to put each of the possible products into perspective.

Sulphide concentrates are usually 'roasted' in conventional fluidised bed roaster technology, using air for oxidation and particle suspension. Roaster products are calcined solids (metal oxides) that can be leached for soluble metal (for example cobalt), which is recovered from solution as an intermediate chemical compound or metal. Roaster off-gas contains heat which could be recovered in a waste heat boiler (and this can be used for electricity

generation) as well as sulphur dioxide gas which can be cleaned and recovered as sulphuric acid.
Thackaringa pyrite could be roasted using this well-tested technology which is operating in South Africa (using wet slurry feed) and in Australia (using dry solids feed).

Autogenous Conditions for Roasting
The reaction of pyrite with air at elevated temperature of 700°C - 750°C is exothermic, autogenous or self-sustaining, without the need for additional diesel (or other fuel) to support continued operation. Typically, a small quantity of fuel is required to elevate the roaster system temperature to the autogenous range, and is not required when roaster reactions become self-sustaining.

This means that dry Thackaringa pyrite can be fed at lower sulphide concentrations to the roaster and water does not have to be evaporated (endothermic) in the roaster. Mathematical modelling of the energy balance for various pyrite-fed fluid bed roasters for dry material indicates approximately 18% sulphide content is required for autogeneity. The roaster operation becomes more sensitive to endothermic reactions involving impurities and any increase in water content as the autogeneity limit is approached. Therefore high-grade pyrite direct feed ore from Thackaringa may have sufficient sulphide content to be suitable dry feed for roasting.

Concentrate Preparation Required for Roasting
For fluid bed roasters, particle size of the feed material is important in terms of the amount of sulphide conversion which is achieved. Feed ore which has been milled to around 60% minus 75 microns with top size of around 300 microns can be roasted efficiently. Larger particles in the feed can be accommodated using a roaster bed overflow system. This means that the coarse particles remain in the fluid bed for a longer time and provided a bed overflow system is installed the coarse calcine product can be separated.

For Thackaringa this means that the pyrite produced has to be comminuted in a dry milling circuit to an appropriate particle size. The pyrite milling circuit can be located at the purchaser's facility and fed directly to the roaster with a reserve silo for pyrite storage to allow for periods of mill maintenance.

Potential Customers

The pyrite product produced by the Thackaringa project has potential uses at several concentrate grades depending on customer requirements. Potential international customers will need to consider additional transport costs and pyrite concentrate grade requirements for off-shore markets are unclear.

GHD undertook preliminary investigations of possible future Australian customers and their likely product requirements. Limited public information is available for some and GHD exercised engineering judgement to assess the likely requirements of several prospective customers.

Potential Customers – General Description
A number of regional businesses have future requirement for sulphuric acid and each provides an opportunity for the Company to supply pyrite for roasting at the consumer's site/s. This approach has the benefit of reducing the extent of processing undertaken by the Company, resulting in lower capital and operating costs.

Production of uranium and copper

A current operating facility producing uranium and copper presently imports sulphur for processing in their acid facility. The sulphuric acid is consumed in their ore-treatment processes. This operation also transports acid from another local refinery to their site. There may be an opportunity to lower costs by using Thackaringa pyrite in the these processes as well as addressing the safety and environmental issues of transporting concentrated sulphuric acid. Based on present acid consumption about 200,000tpa of Thackaringa pyrite would be needed to meet the current sulphuric acid production of this mineral processing operation and this is more than produced in 1.5Mtpa Option 3 or 4 and about 40% of Option 2 production.

Another nearby uranium producer recently demolished their sulphur burner and acid plant and currently imports sulphuric acid.

Several other undeveloped mineral resource projects in eastern Australia will require considerable quantities of sulphuric acid during any future development. The Thackaringa Project is well located to supply these emerging resource projects.

Emerging Producer of Exotic Metals

An advanced project (development approval stage) is planning to import sulphur for burning in a proposed acid plant for use in the processing and recovery of trace elements and metals. The project is located beside rail and road and well positioned to receive pyrite concentrate from Thackaringa. Assuming one cubic metre of acid is required for each tonne of ore then 490,000tpa pyrite could meet the future sulphuric acid requirements of this development.

Fertiliser Production

Superphosphate production requires considerable quantities of sulphuric acid. Phosphate fertiliser production can often be dependent on sulphuric acid supply and cost. Security of supply of Thackaringa pyrite for sulphuric acid generation may attract considerable interest from fertiliser manufacturers in eastern Australia.

Revenue Generation from Cobalt

The importance of potential cobalt revenue should be integral in future development plans. Recent cobalt prices of between A$25,000-A$30,000 per tonne are comparatively low relative to historic prices and cobalt supply and demand issues may have considerable impact on future cobalt price trends (refer notes on cobalt on the last page of this document).

Benefits of a Staged Project Development

The Thackaringa Project may initially consist of a simple low capital cost and low operating cost facility treating high-grade ore (Option 2) with contract mining (perhaps in-pit crushing) to produce a cash flow that, with time, allows further capital investment in a gravity circuit and then a milling and flotation circuit. This will help to optimise mine development and enable more flexibility for differing requirements of a variety of customers.

Processing of concentrate at a facility in the vicinity of Adelaide

GHD investigated a strategy of transporting concentrate to the nearest port (South Australia) by rail (or road). This could allow revenue generation from each of the following:

- Roasting of pyrite to produce sulphuric acid for export or local sale
- Leaching of the calcine (produced from roasting), with sulphuric acid to solubilise Co for recovery and sale (for example as a chemical product)

- Exporting the Fe-calcine to steel mills or cement producer

The pyrite content of the concentrate is important in generating revenue and the following ranking may apply:

- Option 2 has only 35% pyrite in concentrate is unlikely to produce a saleable hematite
- Option 4 with a full gravity circuit (extra capital investment) may not produce a saleable hematite
- Both Option 1 (7.5Mtpa and 1.5Mtpa) include a milling and flotation circuit (increased capital investment) and are most likely to produce a high-iron saleable hematite.

The estimated project values for a process plant located in the vicinity of Adelaide using Option 1 (7.5Mtpa) and Option 1 and 2 (for the 1.5Mtpa throughput) are summarised in Table 5.

For this processing model no Fe-calcine revenue is credited in Options 2 because of the low iron grade of the calcine produced. Also, limited cobalt revenue results from Option 2 because of the relatively low cobalt grade. For Option 2 product stream the capital cost is very high and project value is relatively low.

High pyrite grades in the flotation concentrates in both the 7.5Mtpa and Option 1 (1.5Mtpa) streams may result in much higher revenues. Short payback periods of between 1.6 years and 3.3 years are estimated for these scenarios.

Table 5. Estimated Project Value for an Adelaide processing facility.

Estimated Project Value with external (Adelaide area) processing of product	unit	7.5 Option	1.5 Option 1	1.5 Option 2
Total Operating Costs				
Ore plant and transport	A$ per hour	27943	6536	10592
Concentrate processing	A$ per hour	10340	2063	11250
Total OPEX	A$ per hour	38283	8599	21842
Annual Revenue	A$M per year	335	59	25
CAPEX	A$M	529	198	219
Estimated Project Value				
Payback period	year	1.6	3.3	8.6

Planned Follow-up Programme

BPL is planning a drilling program to test the depth extent of the central part of the Railway Cobalt Deposit in EL6622. This will include diamond drill core sampling through the main envelope of cobalt mineralisation as well as the depth extent of the central portion of the deposit. The drilling will provide suitable drill core sample which can be used for test work to evaluate processing aspects of the mineralisation as well as roasting characteristics of various grades of pyrite content.

Key areas for future work will include resource definition, metallurgical studies mine planning, infrastructure and transport assessment as well as marketing evaluation for cobalt, sulphuric acid and hematite.

Yours faithfully,

Ian J Pringle
(Managing Director)

Competent Person Statement

Exploration activities and results contained in this report are based on information compiled by Dr Ian Pringle, a Member of the Australasian Institute of Mining and Metallurgy. Dr Pringle is the Managing Director of Broken Hill Prospecting Ltd and also a Director of Ian J Pringle & Associates Pty Ltd, a consultancy company in minerals exploration. He has sufficient experience which is relevant to the style of mineralisation and types of deposits under consideration and to the activity which he is undertaking to qualify as a Competent Person as defined in the December 2004 edition of the Australasian Code for Reporting of Exploration Results, Mineral Resources and Ore Reserves (the JORC Code). Dr Pringle has consented to the inclusion in this report of the matters based on his information in the form and context in which it appears.

About Broken Hill Prospecting Limited ("BPL")

BPL is progressing with exploration and evaluation of cobalt-pyrite deposits in the Broken Hill area. Within an exploration tenement (EL6622) and two mining leases (ML86 and ML87) BPL has located cobalt mineralisation (Inferred Mineral Resources) which total 35.7 million tonnes at a combined average grade of 1.85lb/tonne cobalt (Pyrite Hill, Railway and Big Hill deposits) as well as potential mineralisation between 37-59Mt of similar grade at the Pyrite Hill and Railway Deposits (Hellman & Schofield, Nov 2011 and H&SC, July 2012). Exploration for additional cobalt-pyrite mineralisation along-trend and at depth beneath these deposits is in progress.

BPL is in an excellent position to take advantage of an increasing demand for cobalt and sulphuric acid to meet growth in environmental and industrial uses ranging from rechargeable batteries in automobiles to fertiliser production.

BPL is among the next generation of companies that is exploring for major new mineral deposits near the historic western NSW mining centre of Broken Hill, where more than 200 million tonnes of high-grade base metal ore worth an estimated $80 billion has been produced during the past 127 years.

Sulphuric Acid Information

In volume terms, sulphuric acid (H_2SO_4) has the largest world-wide use of any chemical and more than 2,200mt are produced globally each year.

- The production of phosphate fertiliser materials is the major end use for sulphuric acid, accounting for nearly 52% of total world consumption in 2011.
- Other uses include manufacture of plastics, fibres, oil refining, metals and mineral processing.
- Overall, there has been a general increase in demand for sulphuric acid with world consumption increasing by about 58% between 1990 and 2011.
- Future growth in sulphuric acid use is anticipated as increasing populations in developing countries switch to higher nutrition food crops that require soil improvement.
- In a recent report on sulphuric acid supply and demand, HIS Chemical (July 2012) predicted that global demand for sulphuric acid would rise at an average annual rate of almost 2.5% over the next five years.
- Global pyrite production was about 6.7mt (sulphur equivalent) in 2009 and has increased since then. More than 85% is produced and consumed in China.
- Pyrite competes directly with sulphur and by-product sulphuric acid (from smelters and mineral processing). Fluctuations in the availability of these products have a direct impact on the supply and demand of pyrite as well as trade price for concentrate.
- Recent purchases of high-grade pyrite concentrate by the China market have ranged between A$250-A$400/tonne.
- Residue from 'roasted' pyrite concentrate may have considerable commercial value. Cinder which is produced as a very high-iron ash residue after pyrite roasting is extensively used in the cement industry.

Cobalt Statistics

- Cobalt price (LME): US$27,000 per tonne (approximately $14 per pound).
- 1 pound = 0.4536 kilograms
- Mines in Central Africa accounted for over 65% of cobalt production in 2011 and most came from the Democratic Republic of Congo.
- The USA accounted for 58% of cobalt consumption in 2010.
- The USA, Japan, and the European Union have no producing cobalt mines.
- China imported ore from Africa and produced 43% of refined cobalt production in 2010.
- More than 95% of cobalt production is a by-product of copper or nickel mining.
- Lithium-ion batteries contain up to 60% cobalt and will be widely used in the new generation of electric vehicles.
- Cobalt is used in a wide range of industries including production of super alloys and hardened metals where high heat and wear tolerance is required (aircraft, turbines, windmills, military hardware), high-strength magnets, carbides and diamond tools, catalysts (petroleum production), colouring (cobalt blue), adhesive, soaps, driers and food supplements (vitamin B12).

For further information contact;

Dr Ian Pringle, Managing Director, Broken Hill Prospecting Ltd +61 408 548 767
Australian media - Alan Deans, Partner, Last Word Corporate Communications +61 427 490 992

The Company has recently reformatted and updated its website which covers or links to recent news, metal prices, share price as well as project and Company information. Please visit our site at www.bhpl.biz